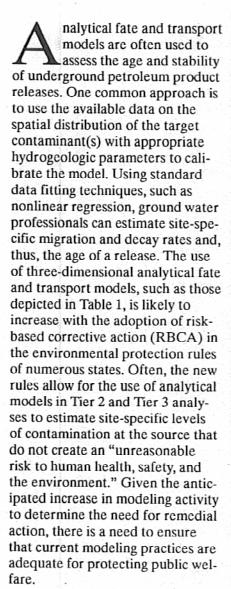
Caution Against the Inappropriate Use of Analytical Fate and Transport Models to Estimate the Age and Risk of Petroleum Product Releases

by Pedro J.J. Alvarez



Hydrogeologists and environmental engineers should ascertain that the ground water flow and contaminant behavior are consistent with the principles used in their analytical models. Unfortunately, this cardinal rule is often forgotten or ignored. Since model simulations are only as good as their input and assumptions, there is a potential for inadvertent misuse of models in negotiating litigation and site-specific target levels under RBCA.

The purpose of this article is to caution interested parties against the inappropriate use of analytical fate and transport models. A case study will be used to illustrate common faults and misjudgments associated with modeling petroleum product releases to ground water. This case study was abstracted from settled litigation. However, the modeling principles discussed apply as well to modeling done for RBCA assessments. This case study emphasizes modeling the fate of benzene, which is often the contaminant of greatest concern because of its potential to cause leukemia (Federal Register 1985).

Case Study

General Background

This case involves a litigation with regard to ground water contamination by a leaking under-

two different operators. Company X operated this facility until 1987. The current operator, Company Y, replaced X's underground storage tank system in 1987. The new system passed all annual tightness tests, and there are no reports of releases or overfills during Company Y's operation. In 1990, gasoline contamination was found by Company Y in an underlying silty bed; a site assessment ensued. Benzene was detected above its maximum contaminant level (MCL) of 5 mg/L in nearby monitoring wells. Nevertheless, no hydrocarbons were detected in the fill sand that surrounds the new UST system. This suggested that contamination occurred prior to the installation of the new UST system in 1987, while Company X operated the facility. Therefore, a cost recovery claim was filed against Company X. In litigation, Company X argued that it was not liable for the contamination observed at this site and hired a consultant to support its defense against the cost recovery claim. The consultant used computer modeling analyses to determine the likelihood that con-

ground storage tank (LUST). The

facility under consideration had

tamination occurred while Company X operated the facility, prior to 1987. Based on a simple fate and transport model, they concluded that "... assuming a pulse source, a single release of benzene dissipates to below the MCL in less than a year. Therefore, any contamination from before 1987 would either

have migrated off-site or degraded by

conclusion is questionable because

model and their choice of benzene

biodegradation coefficient in their

the time samples were collected in

1990." As discussed below, this

of intrinsic limitations on the

applicability of their analytical

Intrinsic Limitations of the Analytical Model

the consultant used an analytical solution to the three-dimensional advection-dispersion equation that

ear partitioning by sorption, and

first-order biodegradation kinetics (Table 1, Equation 1). Similar to most analytical fate and transport models, the principal advantage of this model is its simplicity. This, however, is also its main weakness. While this model is relatively easy to use and requires minimum input of site-specific parameters, there

considers an instantaneous pulse

source, local equilibrium with lin-

are several intrinsic assumptions that should be fulfilled to ascertain its appropriateness and ensure the validity of its output. Nevertheless, data limitations (and perhaps also budgetary constraints) precluded the consultant from determining whether the contamination scenario and the ground water flow acted in a manner consistent with the principles used in the model. Four specific limitations are discussed below. 1. Contamination Source

The consultant concluded that

the benzene contamination

detected within the site must have occurred after 1987 because any prior contamination should have migrated off-site by 1990. Nevertheless, the simulated contamination scenario assumed a single instantaneous pulse source. LUST contamination often resembles a constant source because tanks may leak for an extended period of time, and desorption of hydrocarbons from contaminated soil constitutes another source of sustained ground water contamination. Therefore, the pulse source assumption underestimates the time required for contamination to dissipate by physical processes. A constant source over a stipulated

period may be a more representa-

tive way of modeling LUST con-

tamination. It should be pointed

that introduces error in the time

required for a plume to dissipate.

The consultant assumed a release

of 100 cubic feet, which may or

out that the pulse source analytical

fate and transport simulations. solution requires knowledge of the volume of contaminant released. This is a common uncertainty associated with LUST contamination

To simulate the fate of benzene, 2 = SPRING 1996 GWMR

The model used by the consultant is applicable only to steady

2. Steady Flow

was conservative.

space, the flow does not vary in direction or velocity with respect to time). Often, however, the direction and velocity of ground water flow changes (at least seasonally). In the case under consideration, there was not enough data over time and space to evaluate the validity of the steady flow assumption. Unaccounted fluctuations in ground water flow direction and velocity could result in significant

flow fields (i.e., at any point in

may not be accurate. Additional

information would be required to

determine whether this assumption

this case assumed a uniform flow

3. Uniform Flow

error.

cally assumes homogeneity of the porous medium. Nevertheless, the site under consideration is heterogeneous. Stratigraphic heterogeneities can result in unaccounted

field (i.e., straight and parallel

velocity vectors), which intrinsi-

preferential flow pathways that

predicted and "dead spots" that

transport contaminants faster than

hinder contaminant advection and

where, at any point, contaminant

time. This occurs only under two

ideal conditions: (1) the plume

does not migrate and does not

degrade, at least within the time

frame of the investigation (i.e., the

"trivial" solution); or (2) there is a

constant source, and the migration

rate equals the decay rate so that

there is no net expansion or reces-

SPRING 1996 GWMR = 2

concentrations do not change with

The simulations generated for

Steady state was not an assump-

tion made in this case. Never-

dissipation.

4. Steady-State Plume

theless, this assumption deserves attention because it is commonly

inherent to some fate and transport

analytical models used for RBCA Tier 2 or Tier 3 analyses. By definition, a steady-state plume is one

sion. Often, steady state is assumed for simplicity without establishing the validity of this assumption. Validation of the steady state assumption can be costly because of extensive data requirements over sufficient time and space. Disregarding the validity of this assumption constitutes inappropriate modeling practice that could

Modeling of Benzene Biodegradation

lead to significant error.

Biodegradation is widely recognized as an important mechanism by which benzene is eliminated from LUST plumes (e.g., Barker et al. 1987; Lee et al. 1988; Thomas et al. 1990; Verheul et al. 1988; Werner 1985). While very small gasoline releases could dissipate solely by physical processes such as dilution, one must consider biodegradation to contemplate the possibility that benzene should disappear from typical LUST plumes. Indeed, mass balance studies have demonstrated that "passive" biodegradation (i.e., no biostimulation by oxygen or nutrients addition) is a significant attenuation mechanism in benzene transport (e.g., Chen et al. 1992; Chiang et al. 1989; Klecka et al. 1990; Zoetman et al. 1981). In such cases, biodegradation rates are typically

Bedient 1986). Biodegradation is the only "true" sink considered by most analytical codes. Adsorption, advection, and dispersion do not remove benzene from the aquifer, and volatilization is often (conservatively) ignored in analytical models because it is not a major benzene removal mechanism from dissolved LUST plumes (Chen et al. 1992). Therefore, choosing an appropriate biodegradation model and a reasonable decay rate coefficient is critical to the defensibility of the modeling results.

controlled by oxygen diffusion

from the atmosphere (Borden and

Biodegradation rates are best modeled using Monod kinetics because Monod's equation has a mechanistic (enzymological) basis and considers the active microbial concentration. Therefore, most sophisticated (numerical) fate and transport models use Monod's equation. This equation, however, is hyperbolic and does not yield an explicit analytical solution for the contaminant concentration as a function of time and space. Therefore, simpler (analytical) fate and transport models use empirical kinetic expressions, such as firstorder kinetics (i.e., the rate is proportional to the contaminant concentration) and zero-order kinetics (i.e., the rate is independent of the contaminant concentration). Although benzene biodegradation rates in aquifers have been reported to follow zero-order kinetics (Barker et al. 1987), firstorder rates are more common. This is probably due to the fact that

benzene is often present at trace

concentrations, and Monod's equa-

tion reduces to a first-order expres-

sion whenever the target contami-

nant is present at levels much lower than the half-saturation Monod coefficient, Ks (Alvarez et al. 1991). This condition was met in the case under consideration, and the choice of first-order biodegradation kinetics was appropriate. The choice of first-order biodegradation coefficient, however, was inappropriate. Following common practice, the consultant estimated a first-order biodegradation rate coefficient (λ) of 0.0462 day-1 (i.e., a half-life of 15 days) using site-specific data, and "validated" this coefficient by comparison to values reported in the literature. Nevertheless, the literature values that they considered (Howard et-al. 1991) reflect labora-

tory measurements. Benzene

biodegradation in the field is much

by the rate at which molecular oxy-

gen diffuses into the plume. In situ

rate coefficients are typically one

order of magnitude lower than

their estimated value. A recent

paper by Rifai et al. (1995) pre-

decay coefficients for benzene that

under "passive" conditions. These

literature values have an average

sents a summary of first-order

have been measured at 12 sites

slower because it is often limited

time required for the benzene concentration to drop from 10 mg/L to the detection limit (1 µg/L) in a batch system. In this example, the time required would be 0.55 years using the consultant's estimated coefficient. This is consistent with the consultant's claim that contamination prior to 1987 would have been degraded by 1990. Nevertheless, a time of 14 years would be required if one uses the geometric mean of the literature values reported by Rifai et al. (1995). Therefore, common literature values did not support the consultant's claim of fast (intrinsic) biodegradation. The discrepancy between the estimated and the commonly reported first-order decay coefficients casts doubt on the accuracy of the consultant's fate and transport simulations. While their estimate could have been high due to site-specific conditions (e.g., unlimited oxygen availability, which was not shown), this estimate was based on data from only three monitoring wells. Therefore, the standard error associated with their estimate was relatively large, and most of the literature values reported by Rifai et al. (1995) fell within the 95 percent confidence limit of their estimate. There was also some uncertainty regarding whether the consultant assumed that the concentration of benzene at the source was equal to its solubility in water (about 1780 mg/L). If the source of benzene is gasoline, this assumption would lead to an overestimation of the decay coefficient because the decay curve is forced to begin at an unrealistically high concentration. According to Raoult's law, the concentration of benzene in ground water that is in equilibrium with gasoline cannot exceed the solubil-

of 0.0046 day1 (i.e., a half-life of

0 to 0.0085 day-1 and a geometric

(log) mean of only 0.0018 day-1

149 days) with a common range of

(i.e., a half-life of 375 days). To put

the magnitude of these coefficients

in perspective, let us consider the

ity of benzene in water times its

molar fraction in gasoline (typically

nario assumed a pulse source. When a constant source is assumed, however, the area of the source can be an important factor in estimating the biodegradation coefficient. This situation is often encountered when using models for Tier 2 or Tier 3 (RBCA) analyses, where a finite planar source is often the most realistic geometry

(e.g., Table 1, Equation 2). Care

must be taken not to exaggerate

overestimate the contaminant

thus, it would overestimate the

ulate the observed contaminant

distribution. Similarly, if steady

of the source area (and thus the

mation of the decay coefficient

the area of the source. This would

release rate (i.e., flux times area);

decay coefficient necessary to sim-

state is assumed, an overestimation

release rate) results in an overesti-

necessary to equalize the migration

and degradation rates. An overesti-

mation of the decay coefficient is

conducive to underestimating the

potential health risk associated

with the release because model

distant receptor.

simulations would underestimate

the contaminant concentration at a

The consultant did not evaluate

whether their model was adequately

calibrated with the estimated decay

coefficient (i.e., goodness-of-fit).

was not conducted to assess the

effect of varying the degradation

coefficient within statistical error.

coefficient overestimated the

mated the age of the release.

Consequently, it could not be ruled

out that the selected biodegradation

biodegradation rate and underesti-

Indeed, the best estimate of a given

parameter is not necessarily precise

or reasonable. This is known as the

inverse problem, and it can lead to

models. To prevent this apparently

inaccurate use of mathematical

Furthermore, a sensitivity analysis

about 0.01). This concentration is

al. 1990), but benzene concentra-

tions as high as 130 mg/L can be

achieved with some gasoline for-

The dimensions of the contami-

nation source were not relevant in

this case because the simulated sce-

mulations (Cline et al. 1991).

often less than 20 mg/L (Johnson et

conducive to underestimating the

References

toluene in sandy aquifer mate-

age of the release. Therefore, the that site-specific data used in modeling are valid, and that literature values abstracted for input are owners, operators, and consultants might find themselves in expensive litigation.

Conclusion

out the possibility that the observed contamination occurred prior to 1987, while Company X operated the facility. This conclusion is based on two facts: (1) there was not sufficient data to ensure that ground water contamination and flow acted in a manner consistent with the principles used in their mathematical model; and (2) the instantaneous pulse source assumption and a relatively high

common problem, ground water

adopting compatibility constraints

that limit the input of decay coeffi-

cients. These limits of acceptability

could be based on comparison with

values that have been measured at

similar sites and the relative stan-

dard error of the estimated decay

requirements. Sensitivity analyses

encompassing a reasonable range

of reported values should also be

The modeling work presented

by the consultant could not rule

conducted as routine practice.

coefficient that is necessary to

meet case-specific precision

professionals should consider

modeling defense by Company X was ineffectual. Similarly, for fate and transport modeling under RBCA Tier 2 and Tier 3, the consultant must fully justify that modeling assumptions accurately reflect site conditions,

first-order decay coefficient are

realistic and applicable. Without such detailed justification, risk from exposure to petroleum contamination will likely be erroneously assessed, and LUST site

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Note: The table has been set on the Lino 2000 equipment. A galley will be run from imagesetter for dropin. thanks. merry

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Commonly Used Three-Dimensional Analytical Fate and Transport Models for LUST Releases

in Saturated, Homogeneous Porous Media (Adapted from Dominico and Schwartz 1990) Instantaneous Point Source Model:

Table 1

$$C(x,y,z,t) = K \left[\frac{M}{8 \sqrt{\alpha_x \alpha_y \alpha_z \pi^3 t^3 V r^3}} \right] exp \left[-\frac{(x - v_r t)^2}{4 \alpha_x v_r t} - \frac{y^2}{4 \alpha_y v_r t} - \frac{z^2}{4 \alpha_z v_r t} - \lambda t \right]$$

Where

= 16.019 (i.e., a factor to convert units from lb/ft³ to mg/L)

M = Released mass of contaminant (lbs) (i.e., source concentration times volume released) = Coefficient of longitudinal hydrodynamic dispersion (ft), typically about 25 feet (EPRI 1985) = Coefficient of lateral hydrodynamic dispersion (ft), typically about 5 feet (EPRI 1985)

= Coefficient of vertical hydrodynamic dispersion (ft), typically about 0.5 feet (EPRI 1985) Vr = Retarded velocity of the contaminant (ft/day) (i.e., the average, linear water velocity divided by the

retardation factor)

Constant Source Model:

erf = Error function

 $C(x,y,z,t) = \left(\frac{C_o}{8}\right) \exp\left\{\left(\frac{x}{2\alpha_x}\right) \left[1 - \sqrt{1 + \frac{4\lambda\alpha_x}{Vr}}\right]\right\} \operatorname{erfc}\left[\frac{x - \operatorname{Vr} t \sqrt{1 + 4\lambda\alpha_x/Vr}}{2\sqrt{\alpha_x Vr}}\right]$

 $\left\{ \operatorname{erf} \left[\frac{(y+Y/2)}{2\sqrt{\alpha_y}} \right] - \operatorname{erf} \left[\frac{(y-Y/2)}{2\sqrt{\alpha_y}} \right] \right\} \left\{ \operatorname{erf} \left[\frac{(z+Z/2)}{2\sqrt{\alpha_z}} \right] - \operatorname{erf} \left[\frac{(z-Z/2)}{2\sqrt{\alpha_z}} \right] \right\}$

Where all variables are as previously defined and

= Contaminant concentration at source (mg/L) = Source width (ft) (i.e., depth of the soil source, if contaminated soil exists, or the width of the tank

excavation if no contaminated soil exists) = Source depth (ft) (i.e., depth of the soil source, if contaminated soil exists, or the depth of the fill excavated below the tank if no contaminated soil exists)

erfc = Complementary error function = 1 - erf

= Site-specific first-order decay coefficient (day-1)

(2)

(1)

= Contaminant concentration (mg/L) at a longitudinal distance of x feet, a transverse (lateral) distance of y feet, and a depth of z feet from the source, at time t (days) after the release